

DISTURBANCE REJECTION WITH A HIGHLY OSCILLATING SECOND-ORDER-LIKE PROCESS, PART VI: PPI CONTROLLER

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Abstract— *A PPI controller is investigated for disturbance rejection associated with a highly oscillating second-order-like process. The controller is tuned using the MATLAB optimization toolbox for different error-based objective functions. The best objective function suitable for this type of controllers for the highly oscillating second order process is assigned. The unit step disturbance input time response of the control system has zero steady-state error and low response levels. The effect of the proportional gain of the PPI controller on the system dynamics is investigated. The PPI controller when used for disturbance rejection associated with the highly oscillating second-order process can compete well with PD-PI and PI-PD controllers used for the same purpose.*

Keywords— *Disturbance rejection, PPI controller, second-order-like process, controller tuning.*

I. INTRODUCTION

This is the six paper in a series of research papers aiming to investigate specific controllers and compensators for disturbance rejection associated with second-order-like processes having high oscillation nature. The resulting control system has to be stable and capable of rejecting the disturbance input with good performance measures.

Rada and Lo (1994) proposed using a predictive proportional integral controller with improved performance. They realized the PPI controller by continuous time implementation [1]. Ren, Zhang and Shao (2003) demonstrated the performance of PPI controller and showed that the PPI controller is suitable for long time delay processes and has excellent robust stability. They compared its performance with traditional PID controller using different tuning methods [2]. Larsson (2011) optimized PID and PPI controllers with measurement filters. He compared using the presented control signal activity constraint and robustness margins [3].

Airikka (2012) presented a modification of a PPI controller to deal with processes with long dead times. His proposed method had resemblance with PID controller and was applicable for industrial dead time dominating processes [4]. Airikka (2012) suggested an event-based control strategy for predictive PI controllers to solve the problem of material transportation time delay in mobile crushing plants [5]. Larsson and Hagglund (2012) presented a performance comparison between PID and PPI controllers. They performed optimization of controller and measurement filter parameters considering load disturbance rejection, robustness and noise sensitivity for a batch of industrial processes [6]. Ribic and Matausek (2012) proposed a PPI controller applied to the benchmark MIMO PID 2012. They proposed tuning rules for stable, integrating and unstable processes. They demonstrated the high performance of the proposed PPI controller with additional filtering [7]. Airikka (2013) analysed in details the stability of the PPI control loop for accurate process models having no model mismatch and processes having modelling errors and uncertainties. He has given some preliminary guidelines for the controller tuning [8]. Shihe et. al. (2014) introduced a control strategy based on active disturbance rejection control to the Shell gasifier control system. Their control system has shown advantages of better reference-tracking and disturbance rejection capability, strong robustness and easy tuning procedure compared with PI controllers with probabilistic robustness [9].

Shinde, Waghmare and Hamde (2014) introduced a model reference learning approach with PPI control strategy for higher order systems. They compared their results with other PPI control methodologies showing good tracking performance than other PPI controllers with minimum reaching time [10]. Hassaan (2015) investigated using a PPI controller for set-point tracking associated with a highly oscillating second-order-like process. He tuned the PPI controller using MATLAB toolbox and five objective functions. He could reduce the maximum overshoot of the step time response of the control system using the PPI controller to zero. He compared the control system performance with control systems using I-PD, PD-PI, PI-PD, PID + first-order lag and PID controllers [11].

II. Process

The process is a second-order like one without time delay having the transfer function, $G_p(s)$:

$$G_p(s) = \omega_n^2 / (s^2 + 2\zeta\omega_n s + \omega_n^2) \quad (1)$$

Where:

$$\omega_n = \text{process natural frequency in rad/s} = 10 \quad \text{rad/s} \quad \zeta = \text{process damping ratio} = 0.05$$

This process has a maximum overshoot of 85.4 % indicating the high oscillation nature of the process.

III. The ppi controller

The block diagram of a linear feedback control system for set-point tracking exhibiting a PPI controller is shown in Fig.1 [12].

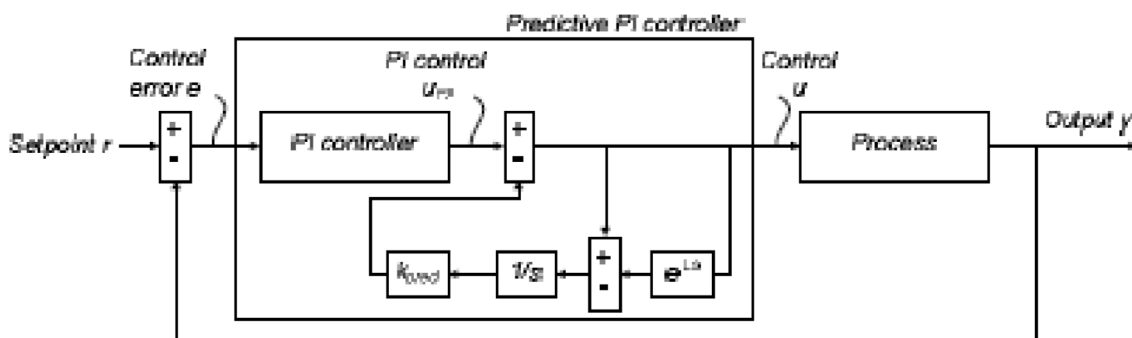


Fig.1 PPI controller in a control system for set-point tracking [12].

The PI controller part in Fig.1 is a standard PI controller having the transfer function, $G_{PI}(s)$:

$$G_{PI}(s) = K_{pc} + K_i/s \quad (2)$$

According to Airrikka, the PPI controller of the structure shown in Fig.1 has an overall transfer function between its output $U(s)$ and input $E(s)$, $G_{PPI}(s)$ given by [12]:

$$G_{PPI}(s) = s(K_{pc} + K_i/s) / \{s + K_{pred}[1-\exp(-Ls)]\} \quad (3)$$

Where:

K_{pc} and K_i are the proportional and integral gain coefficients of the PI controller. K_{pred} is the predictive gain coefficient of the feedback element shown in Fig.1.

L is the time delay of the PPI controller in the feedback element shown in Fig.1.

To facilitate the dynamic analysis of the control system, the first-order Taylor series is used to replace the exponential term in Eq.3 by a first-order polynomial. That is [13]:

$$\exp(-Ls) \approx -Ls + 1 \quad (4)$$

Combining Eqs.3 and 4 gives:

$$G_{PPI}(s) = (K_{pc} + K_i/s) / [1+K_{pred}L] \quad (5)$$

The term $1 + K_{pred}L$ in Eq.5 is a constant parameter independent of the Laplace operator s . Therefore, it can be replaced with one parameter K' . That is:

$$G_{PPI}(s) = (K_{pc} + K_i/s) / K' \quad (6)$$

IV. Closed-loop transfer function

The closed loop transfer function of the closed loop control system depends on the input and output variables of the control system. With disturbance input included in the analyses, the control system has two input variables: reference input $R(s)$ and disturbance input $D(s)$ as shown in Fig.2.

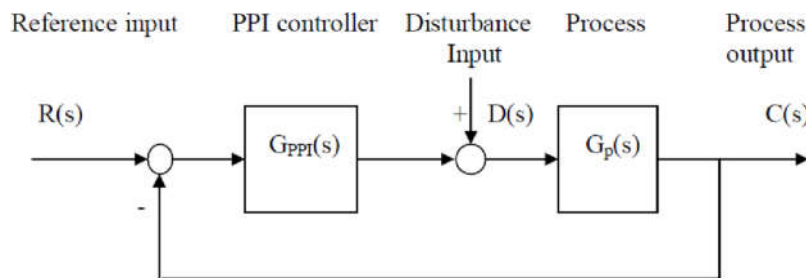


Fig.2 System block diagram with two input variables.

For sake of studying the dynamics of the control system for disturbance rejection, only the disturbance variable $D(s)$ has to be considered, and the reference input will be omitted from Fig.2. In such a case, the controller block will come in the feedback path of the single loop of the control system and the controller output signal will enter the error detector (summing point) with a negative sign. The transfer function of the control system in this case, $C(s)/D(s)$ considering Eqs. 1 and 6 will be:

$$C(s)/D(s) = b_0s / (s^3+a_0s^2+a_1s+a_2) \quad (7) \text{ Where:}$$

$$b_0 = \omega_n^2$$

$$a_0 = 2\zeta\omega_n$$

$$a_1 = \omega_n^2 (1 + K_{pc} / K')$$

$$a_3 = \omega_n^2 K_i / K'$$

V. CONTROLLER TUNING

Tuning of the PPI controller for disturbance rejection of the highly oscillating second-order process allows adjusting the controller three parameters K_{pc} , K_i and K' for optimal disturbance rejection. The desired steadystate response for disturbance rejection is zero. This allows us to define an error function $e(t)$ as the time response to the unit disturbance input. That is:

$$e(t) = c(t) \quad (8)$$

The controller tuning is performed using the error function of Eq.8 which is incorporated in an objective function to be minimized using the MATLAB optimization toolbox [14]. The objective functions used are ([15][17]):

$$\begin{aligned} \text{ITAE: } & \int t|e(t)| dt & (9) \\ \text{ISE: } & \int [e(t)]^2 dt & (10) \\ \text{IAE: } & \int |e(t)| dt & (11) \\ \text{ITSE: } & \int t[e(t)]^2 dt & (12) \\ \text{ISTSE: } & \int t^2[e(t)]^2 dt & (13) \end{aligned}$$

The tuning results for a control system incorporating the PPI controller and the highly oscillating secondorder-like process for disturbance rejection are given in Table 1.

TABLE 1 PPI CONTROLLER TUNING AND CONTROL SYSTEM PERFORMANCE FOR DISTURBANCE REJECTION

	ITAE	ISE	IAE	ITSE	ISTSE
K_{pc}	500	500	500	500	500
K_i	1.1019	1.1019	0.10	0.10	1.1003
K^o	3.9745	3.9749	3.9917	4	3.9751
c_{max}	0.0077	0.0077	0.0077	0.0077	0.0077
T_{cmax} (s)	12.1157	12.1157	133.44	133.28	12.1338

It is clear from the tuning results in Table 1 that the ITAE, ISE and ISTSE objective functions generates almost the same optimal time response while the IAE and ITSE generate another optimal sluggish time response.

VI. CONTROL SYSTEM TIME RESPONSE

The time response of the control system for a unit step disturbance input for the five objective functions of Eqs.9 to 13 is shown in Fig.3.

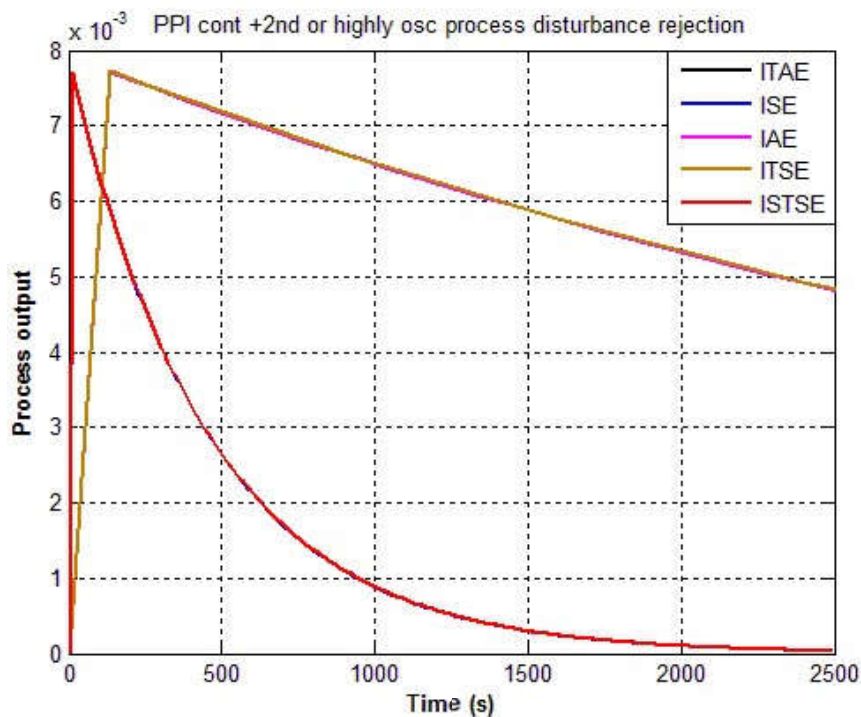


Fig.3 Unit step disturbance input time response using a PPI controller.

Fig.3 indicates that the step time response is smooth, has a small level and decays to zero in a very long time. However, it has a zero settling time as it is less than an 0.05 value.

VII. Effect of controller proportional gain k_{pc}

Different levels of the proportional gain K_{pc} are tried keeping the other optimal values in Table I. Since the optimization problem of the tuning process is nonlinear in the controller parameters, local minima are expected. Different levels of K_{pc} are tried keeping the other PPI controller parameters at the levels in Table I. The simulation results investigating this effect are shown as an effect of the time response of the control system due to the unit step disturbance input shown in Fig.4.

It is clear from Fig.4 that K_{pc} has a great effect on the disturbance rejection process. It is possible to decrease the maximum time response value from 0.0077 to 0.00096 by increasing the gain K_{pc} from 500 to 4000

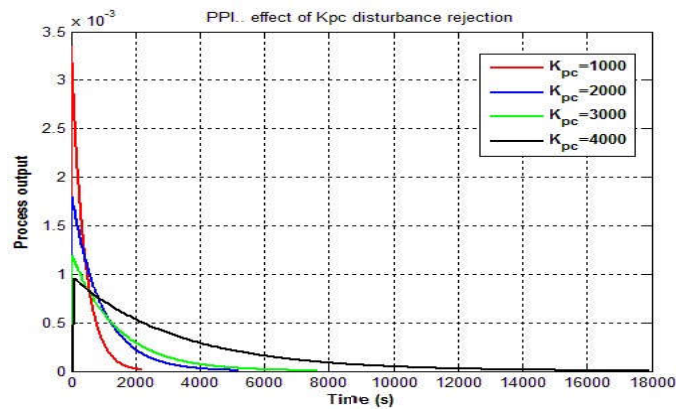


Fig.4 Effect of K_{pc} on the unit step disturbance input time response.

The effect of the PPI proportional gain is further investigated through the maximum time response, c_{max} and its time, T_{cmax} . This effect is illustrated graphically in Fig.5 for proportional gain in the range: $500 \leq K_{pc} \leq 4000$.

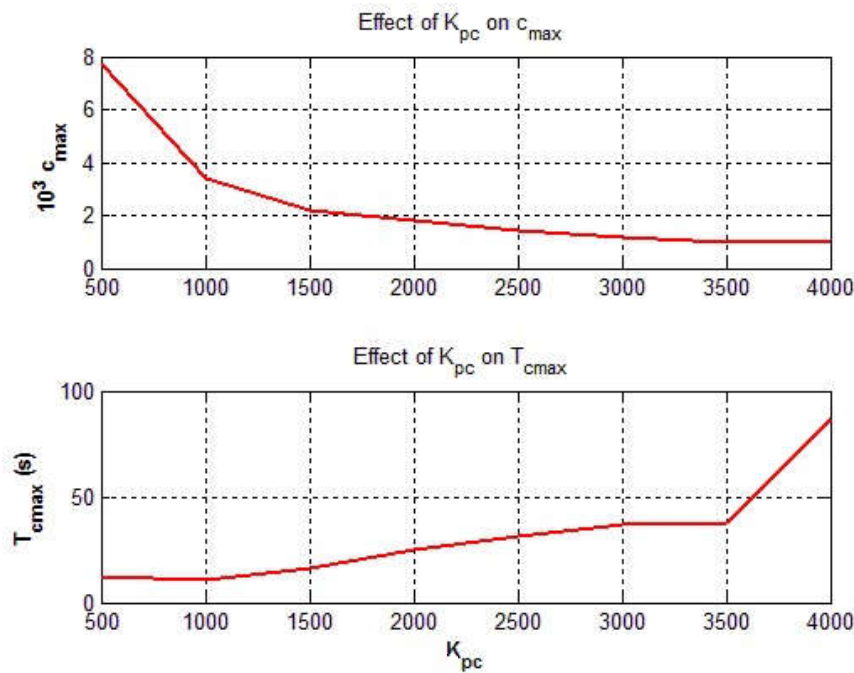


Fig.5 Effect of K_{pc} on the maximum time response and its time.

It is clear how the maximum time response decreases as the proportional gain increases while the time of the maximum response increases as the proportional gain increases.

VIII. Comparison with other controllers

To investigate the effectiveness of using a PPI controller for disturbance rejection associated with a secondorder-like highly oscillating process it is compared with that of using PD-PI [18], PI-PD [19], IPD [20] and 2DOF [21] controllers for the same process.. The unit step disturbance input time response of the control system using the compared five controllers is shown in Fig.6.

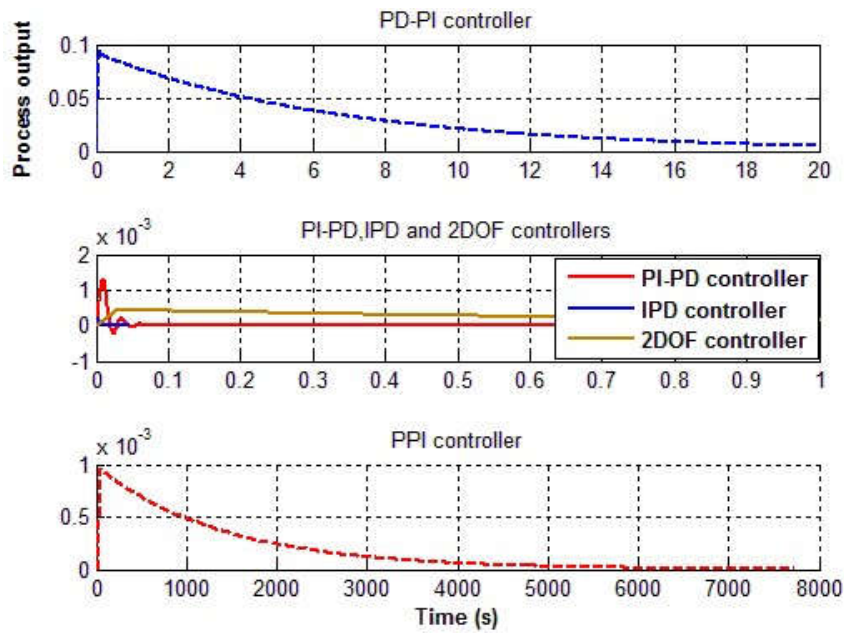


Fig.6 Comparison of the unit step disturbance input time response.

The control system performance for disturbance rejection is compared in Table 2 between the PPI and the other four controllers.

TABLE 2 PERFORMANCE COMPARISON

	c_{max}	T_{cmax} (s)
PD-PI controller	0.0950	0.1200
PI-PD controller	0.0013	0.0100
IPD controller	$1.927 \cdot 10^{-4}$	0.0036
2DOF controller	$5.113 \cdot 10^{-4}$	0.0079
PPI controller (present)	$9.60 \cdot 10^{-4}$	37.580

IX. Conclusions

- A PPI controller was investigated for disturbance rejection associated with a highly oscillating secondorder- like process.
- The controller was tuned using MATLAB optimization toolbox and five different objective functions.
- The ITAE, ISE and ISTSE objective functions gave the same effect on the time response of the control system.
- The effect of the proportional controller of the PPI controller on the disturbance time response was investigated where it had a remarkable effect on the time response due to disturbance input.
- The PPI controller could go down with the maximum time response value to as low as $9.6 \cdot 10^{-4}$..
- The time response to a step disturbance input was sluggish within its very small value.
- Comparing with the research work using PD-PI, PI-PD, IPD and 2DOF controllers, the PPI controller could compete with the PD-PI and PI-PD controllers regarding the maximum time response value.

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